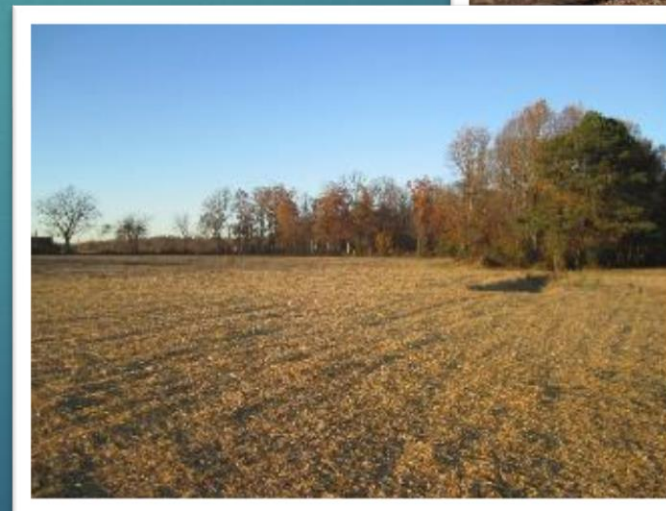


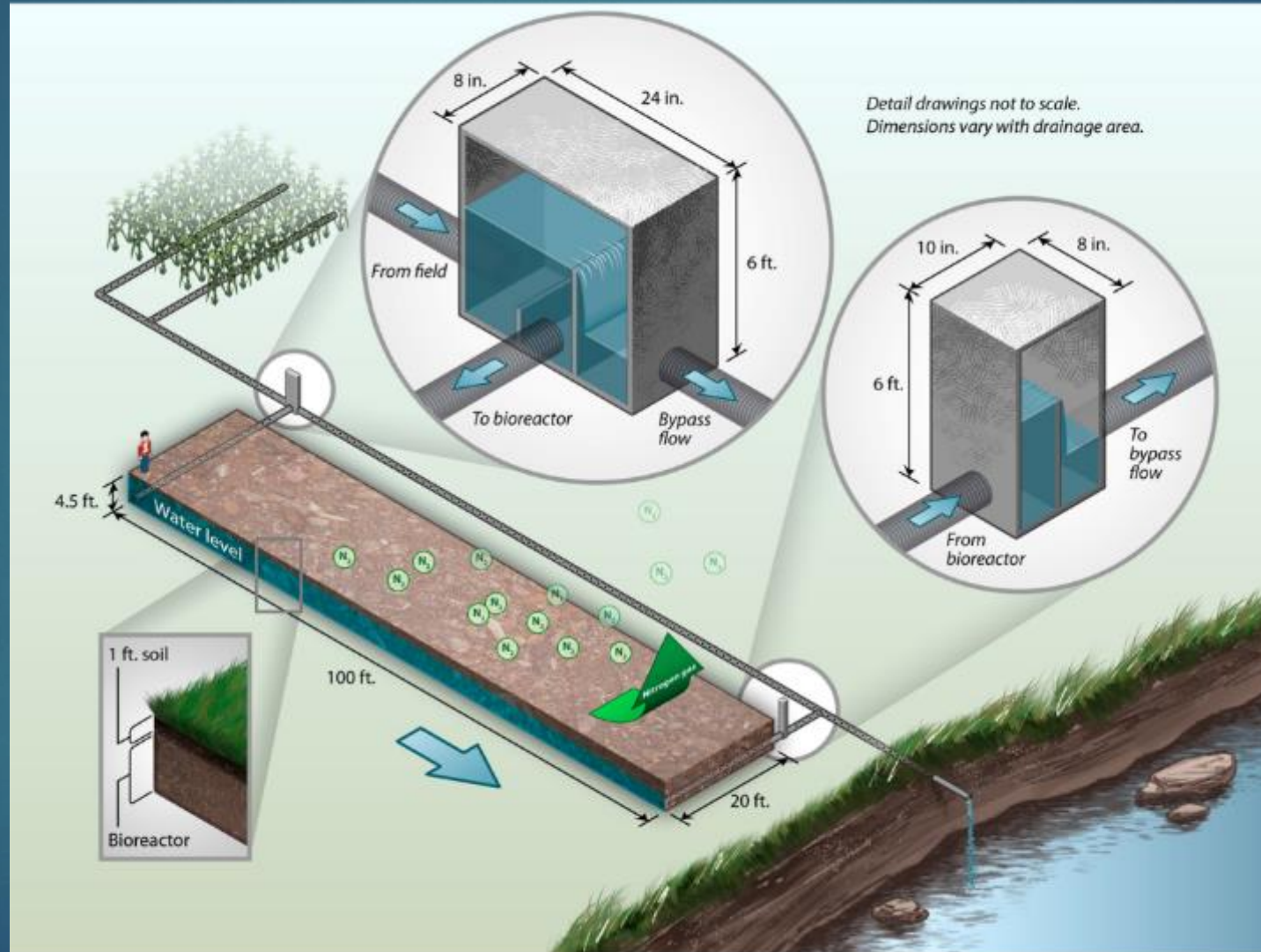
# Conservation Drainage

## Denitrifying Bioreactor

Timothy Rosen, Watershed Scientist  
Midshore Riverkeeper Conservancy



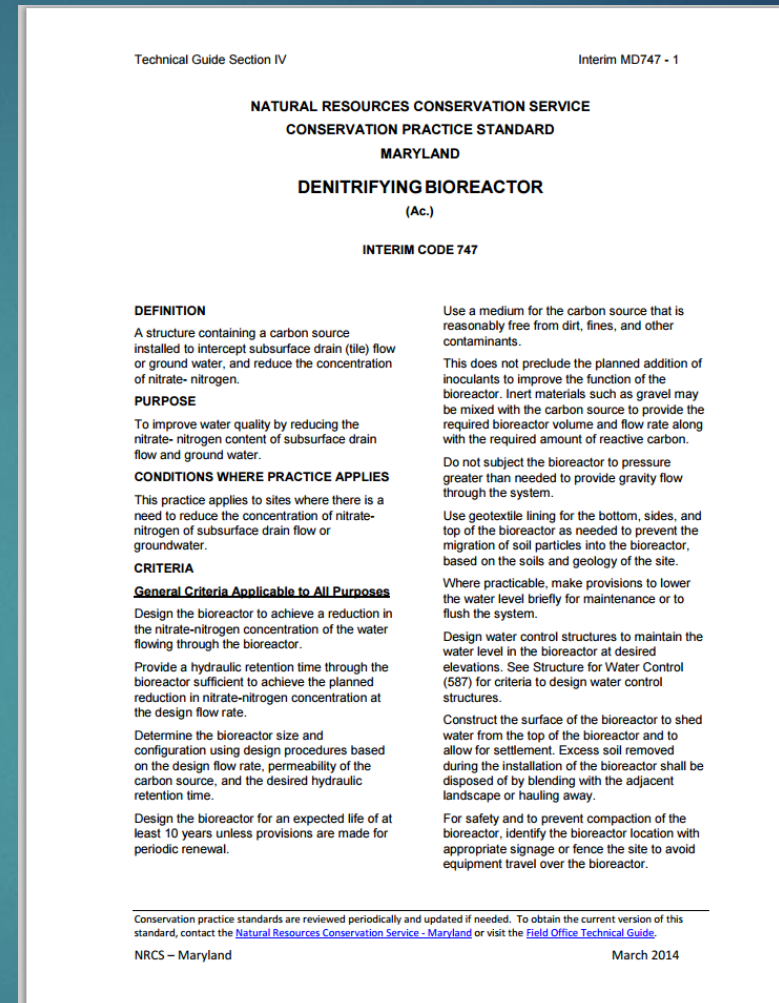
# Denitrifying Bioreactor





# Overview

- ▶ Implemented/studied in Midwest
- ▶ NRCS Standard
- ▶ 10 year lifespan
- ▶ Data collection at 7 sites on the eastern shore of Maryland
- ▶ Implemented in 3 Chesapeake Bay states: NY, VA, MD



# Engineering Guide

Subsurface Drainage Bioreactor Design

Developed by M. Helmers & L. Christianson, ABE, Iowa State University

Modified for NRCS use by B. Atherton, P.E., Agricultural Engineer

laDenitrifyingBioreactor.xls Ver 1.0

Instructions: Enter values in gray cells

Field Information:

Tile Size (in)	6
Tile Grade (%)	0.50
Manning's "n" value	0.015
Velocity in Pipe (ft/s)	1.76
Peak Flow from Tile Size (cfs)	0.345

Media Information:

Conductivity of Wood Media (ft/s) (K)	0.15
Porosity of Wood (p)	0.7

Bioreactor Inputs and Calculations:

Flow Length (ft) (L)	100
Trench Width (ft) (W)	10
Inlet Height (ft)	2.5
Outlet Height (ft)	0.3
Head Drop (ft) (ΔH)	2.2
Flow Depth (ft) (d)	1.4
Hydraulic Gradient (i)	0.022

Results:

Bioreactor Flow Rate (cfs) (Q)	0.045
Hydraulic Retention Time (hours) (HRT)	6.0
% of peak flow that can be passed through bioreactor	13.2

Explanatory Notes:

Size of inflow tile; known from site

Limiting Grade of inflow tile; known from site

3" - 6" Corrugated Plastic Pipe (tubing), single wall

Mannings Gravity Driven Flow Equation =  $1.49 \times \sqrt{\left(\frac{\text{Tile Grade}}{100}\right)} \times \frac{\left(\frac{\text{Tile Size}}{\text{(Conversion)}}\right)^{2.63}}{0.012(\text{for dual wall}) \text{ OR } 0.015(\text{for non-dual walled})}$

Flow rate = Velocity x Area of Tile

Converted from 4.5 cm/s per Laura Christianson; (original value 9.5 cm/s to ft/s; value determined in Porous Media Lab, AB

Taken from van Driel et al., 2006

Iteratively choose to the nearest foot

Iteratively choose to the nearest foot; should be less than 25% of the flow length

Iteratively choose to the nearest 0.1 foot

Iteratively choose to the nearest 0.1 foot

Calculated based on difference between inlet and outlet

Calculated to be in bioreactor middle (average of inlet and outlet height)

Head Drop / Flow Length

Darcy's Law for Porous Media Flow =  $\text{Hyd. Conductivity} \times \text{Hyd. Gradient} \times \text{Flow Area} = KiA = Ki(W \times d)$

$\text{HRT} = \tau = \frac{\text{Volume} \times \text{porosity}}{\text{Flow rate}} = \frac{Vp}{Q} = \frac{L \times W \times d \times p}{Q}$  (conversions included); 4 hour min., should be 6 to 8 hours

Bioreactor Flow Rate / Peak Flow from Tile ; minimum 15%

Ground Surface

Inlet Water Control Structure (WCS)

Outlet WCS

Backfill Soil

Wood Chip Trench

Inlet Height

Head Drop

Outlet Height

Flow Depth

Flow Length

Flow

Inflow Tile Size (in)

Outlet

Schematic — Not to Any Scale

Notes:

This Bioreactor design is based on treating a minimum of 15% of the peak flow capacity of the drainage system.

The design retention time is between 4 - 8 hours (Robertson et al., 2000; van Driel et al., 2006).

The logo for Midshore Riverkeeper Conservancy is an oval emblem. It features a stylized bird in flight above the word "RIVERKEEPER" in a serif font. Below this, there is a depiction of green grass. The words "MIDSHORE" and "CONSERVANCY" are written in a sans-serif font along the top and bottom inner edges of the oval, respectively.

# Background

Before Construction





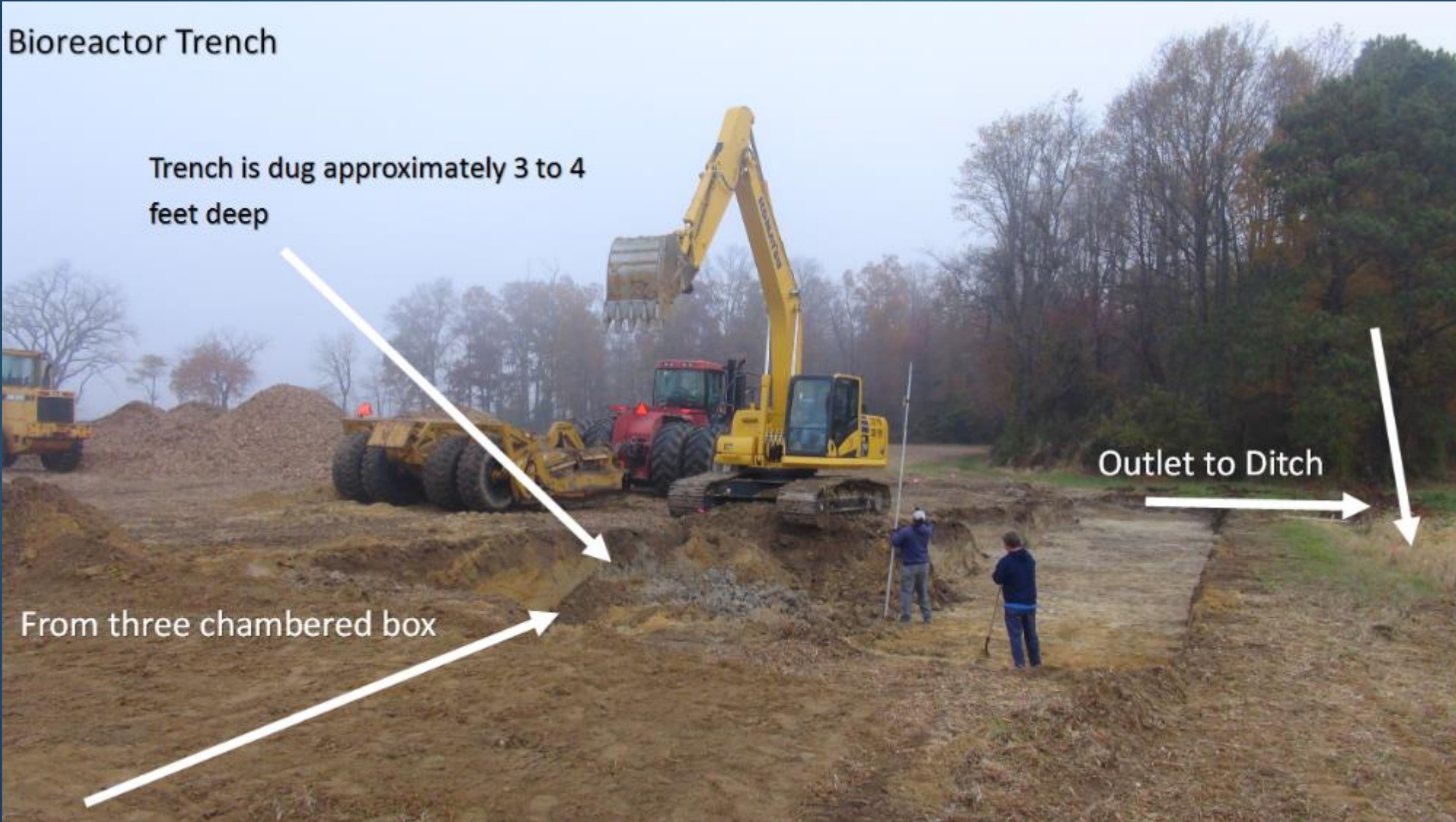
# Background





# Background

## Bioreactor Trench





# Background





# Background





# Background

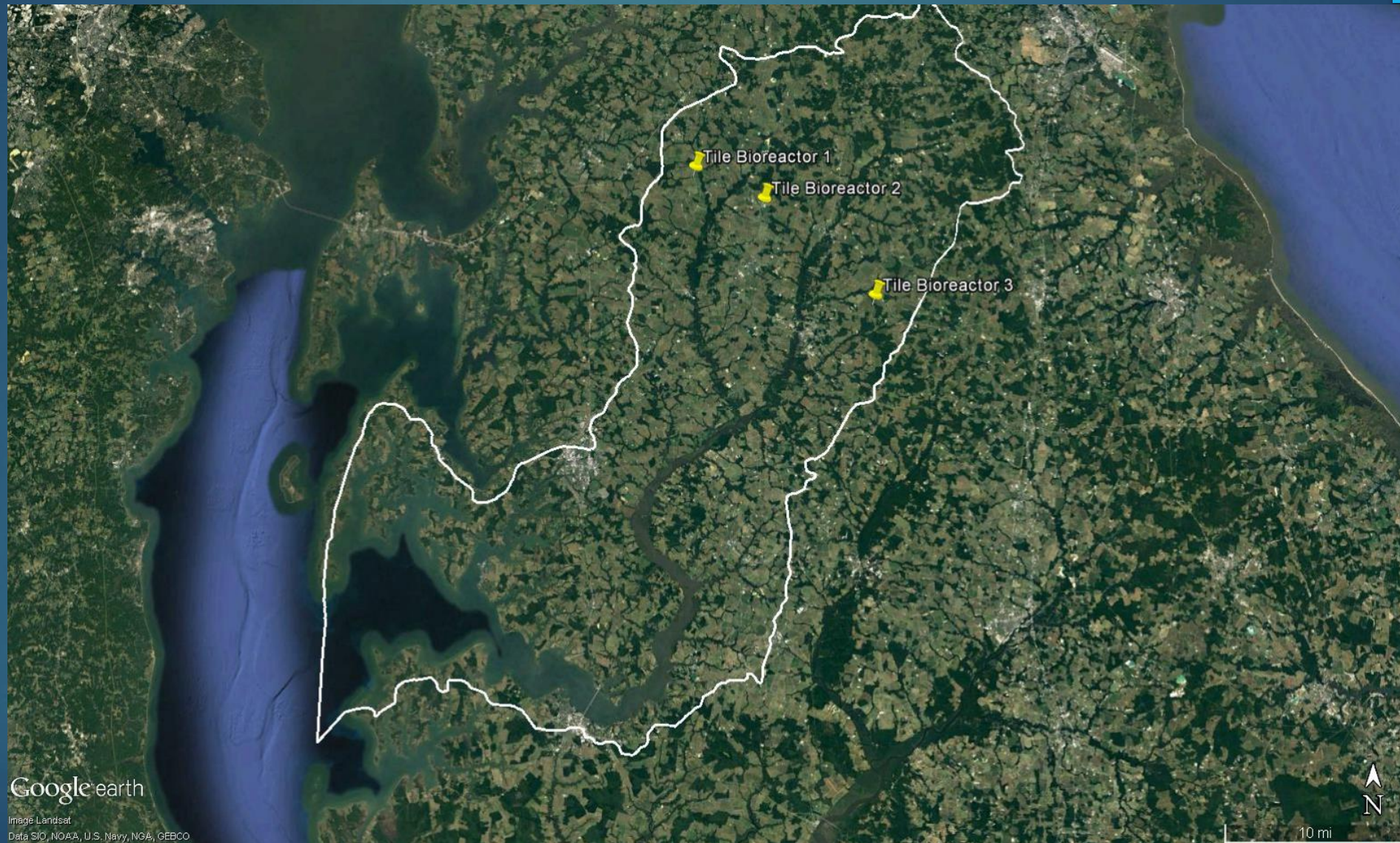


Trench is backfilled to  
surface elevation on the  
edge with slight crown in  
center



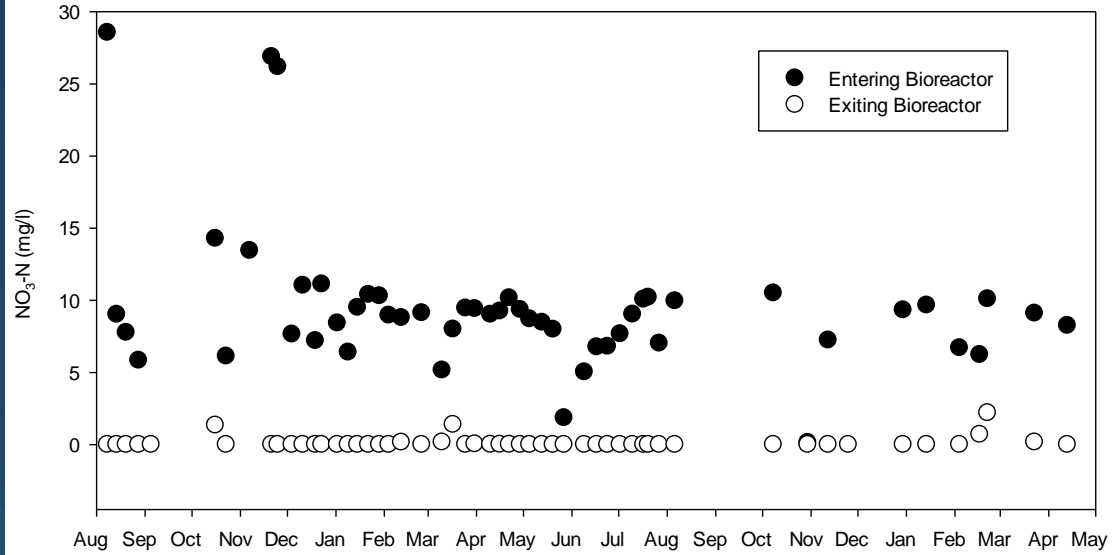


# Locations

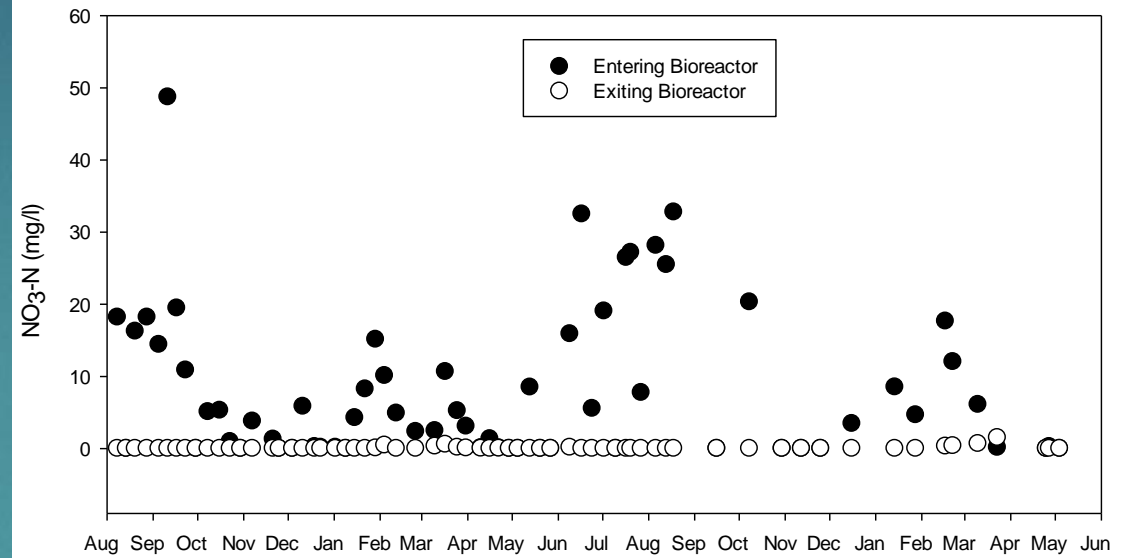


# Results- Nitrate

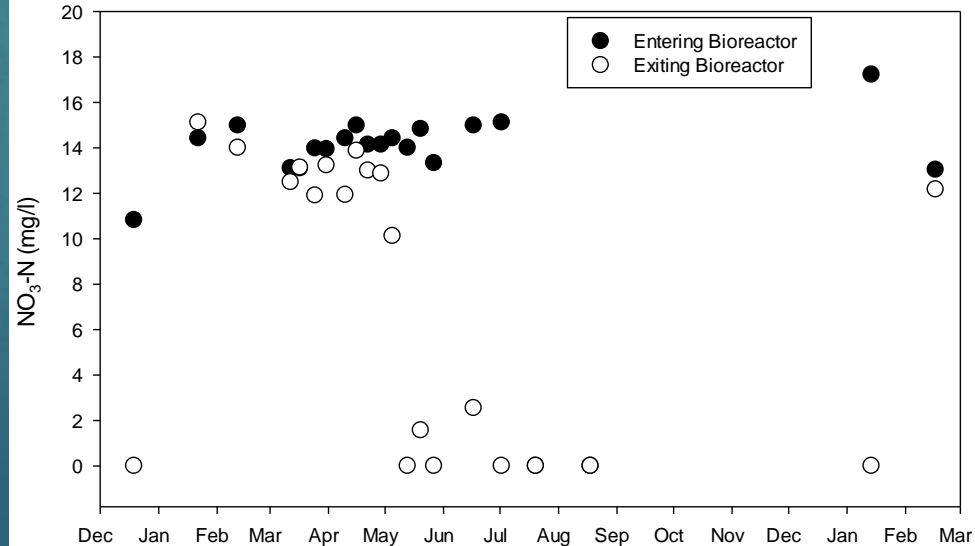
## Bioreactor 1



## Bioreactor 2



## Bioreactor 3





# Results

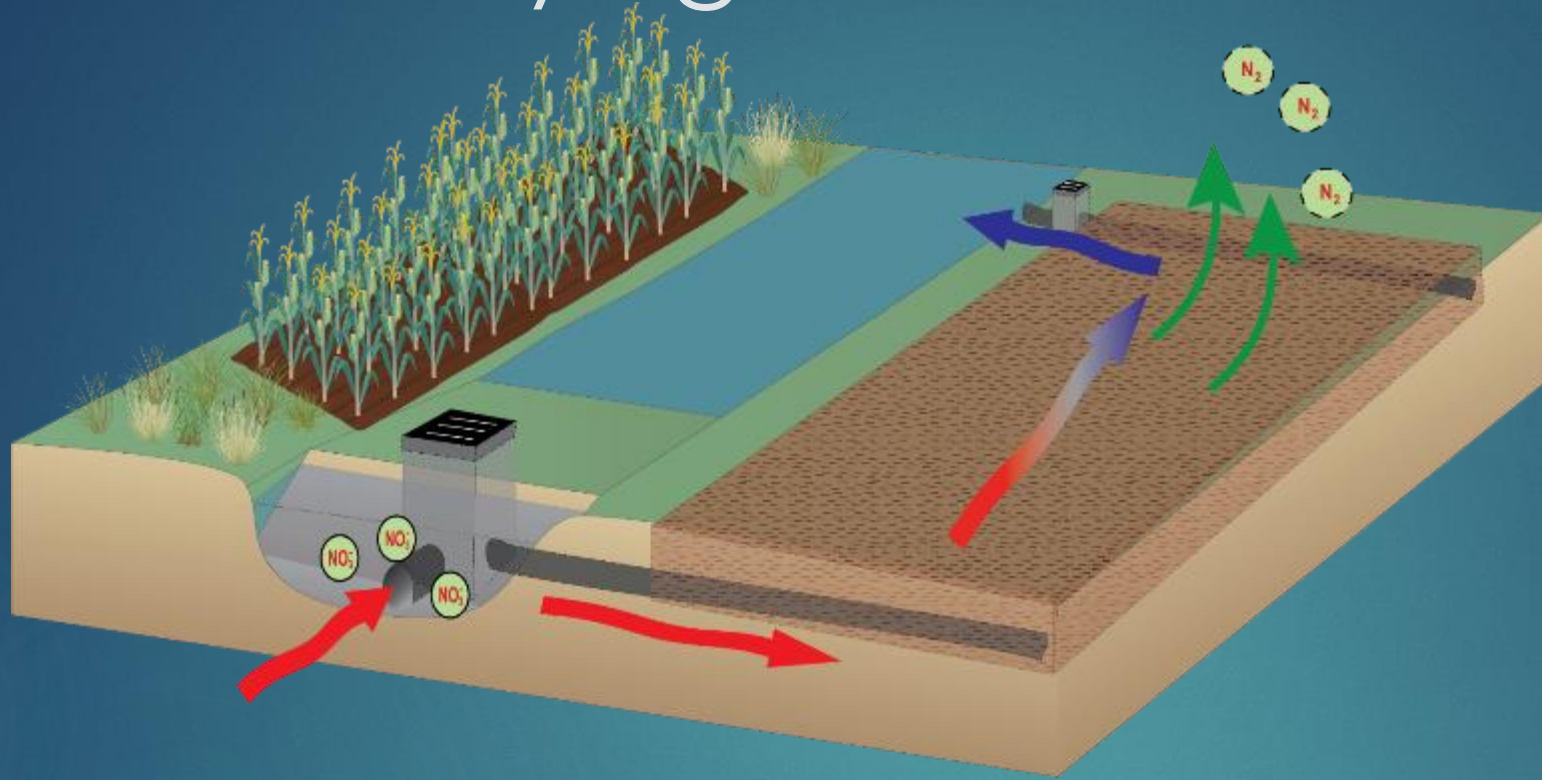
	Flow		Bioreactor						Total (including by-pass flow)		
	Total volume from field	Percent treated in bioreactor	Flow weighted concentration: IN	Flow weighted concentration: OUT	Nitrate load: IN	Nitrate load: OUT	Nitrate removal efficiency	Nitrate removal rate†	Nitrate load: IN	Nitrate load: OUT	Nitrate removal efficiency
	m <sup>3</sup>	%	----- mg NO <sub>3</sub> -N/L -----		----- kg N -----		%	g N removed per m <sup>3</sup> bioreactor per d	----- kg N -----		%
Bioreactor 2											
8 Aug 2014-6 Aug 2015	37,000	13%	4.65	0.06	23	0.3	99%	<b>0.40</b>	251	229	<b>9.0%</b>
6 Aug 2015-22 Feb 2016 ‡	4,460	18%	9.43	0.11	7.7	0.1	99%	<b>0.24</b>	51	43	<b>15%</b>
Bioreactor 1											
8 Aug 2014-6 Aug 2015	18,400	63%	8.94	0.10	103	1.1	99%	<b>3.43</b>	158	57	<b>64%</b>
6 Aug 2015-30 Oct 2015 ‡	870	77%	7.69	0.39	31	1.6	95%	<b>2.23</b>	8.7	2.1	<b>76%</b>
Bioreactor 3											
19 Dec 2104-20 Jul 2015‡	49,700	98%	13.46	11.57	677	607	10%	<b>1.53</b>	688	618	<b>10%</b>

# Results

	----- Nitrate-N -----		----- Ammonium -----		----- Total Nitrogen -----		-- Orthophosphate --		----- Total Phosphorus -----			
	----- mg N/L -----								----- mg PO <sub>4</sub> /L -----		----- mg TP/L -----	
	Inflow	Outflow	Inflow	Outflow	Inflow	Outflow	Inflow	Outflow	Inflow	Outflow		
Bioreactor 2	8.73 ± 10.7 (61) †	0.04 ± 0.1 (61) †	9.74 ± 11.1 (36)	14.3 ± 16.9 (36)	28.3 ± 20.6 (18) †	12.3 ± 7.3 (18) †	2.33 ± 2.7 (36)	1.61 ± 2.1 (36)	4.77 ± 4.8 (18)	3.22 ± 3.0 (18)		
Bioreactor 1	9.52 ± 5.1 (50) †	0.12 ± 0.4 (51) †	0.23 ± 0.7 (30)	0.27 ± 0.5 (30)	11.7 ± 6.1 (14) †	2.47 ± 2.2 (14) †	0.16 ± 0.3 (30)	0.22 ± 0.4 (30)	0.61 ± 0.7 (14)	0.61 ± 0.8 (14)		

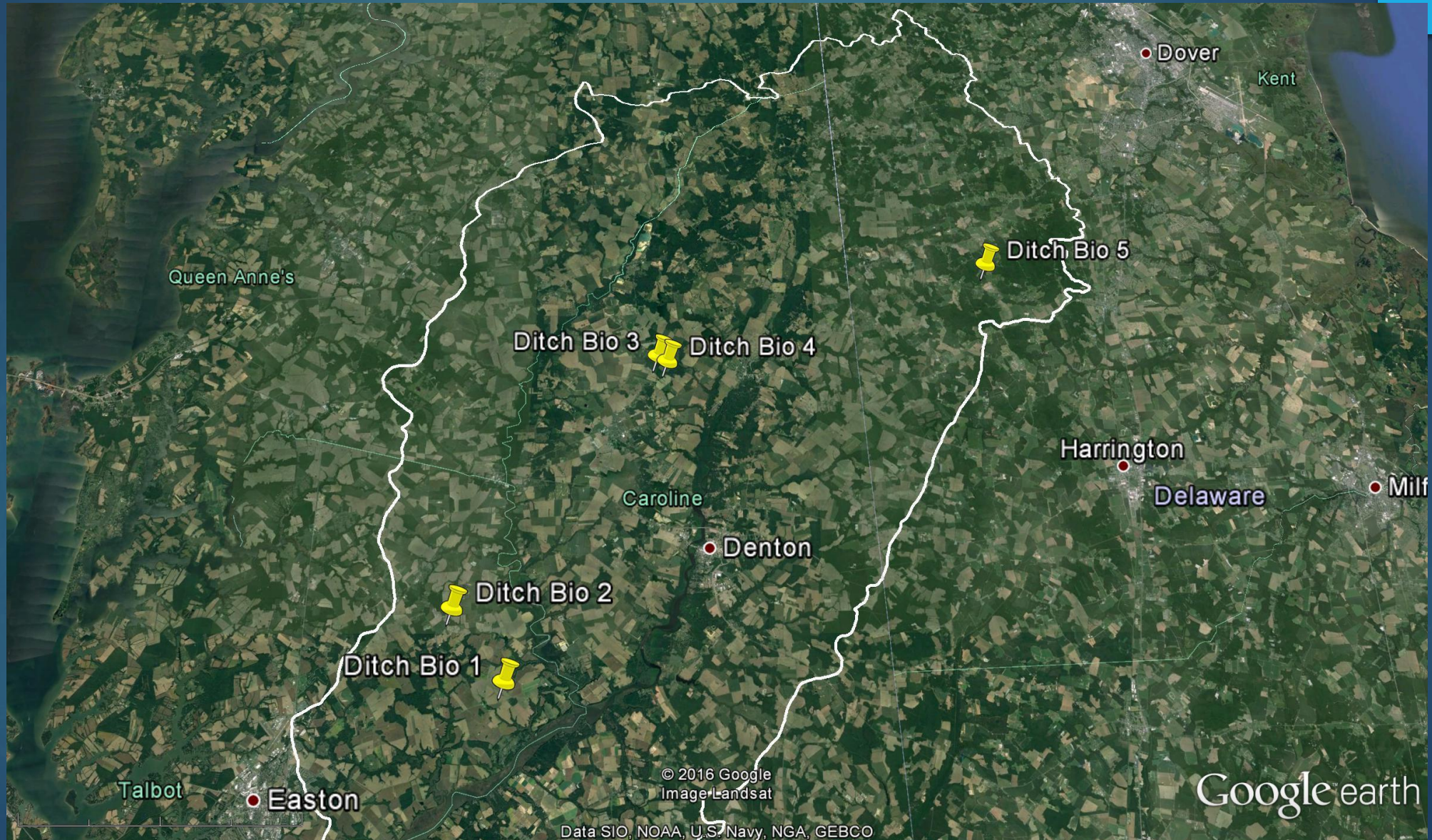


# Ditch Denitrifying bioreactor





# Locations



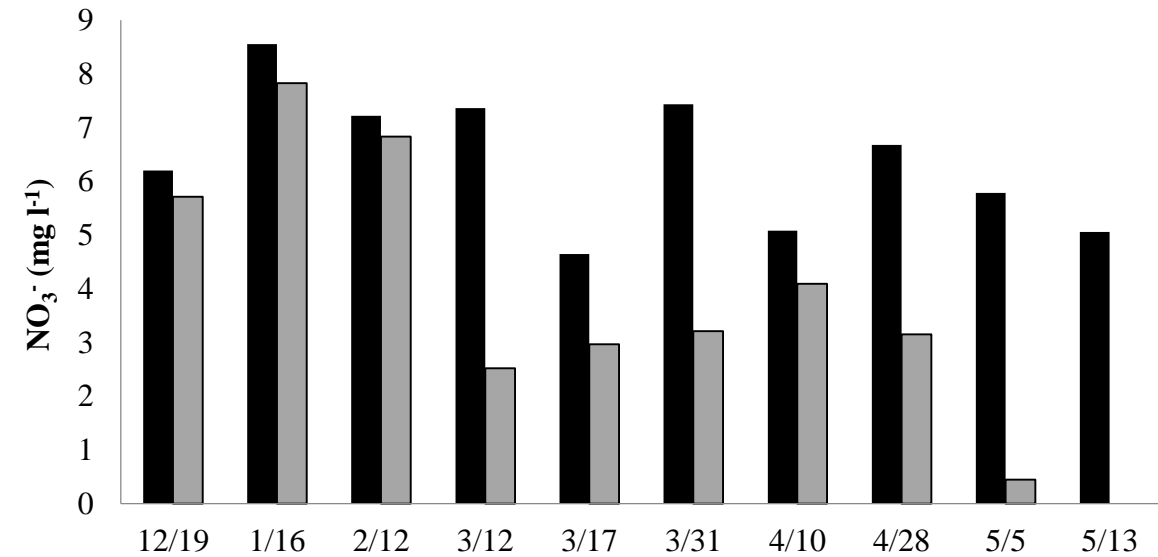
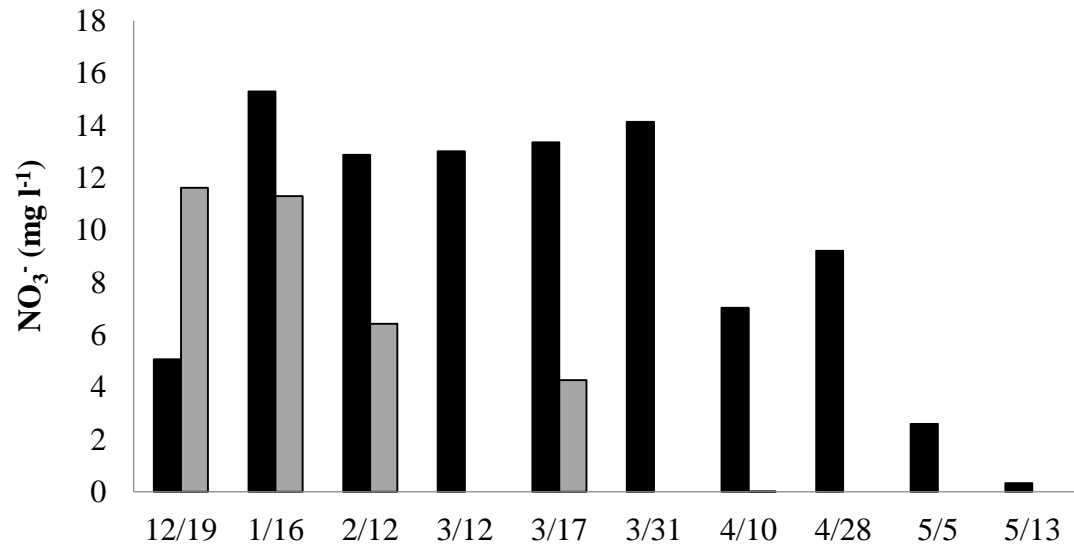


# First and Second Generation



# First Generation

## Nitrate Reduction (mg/l)-Base Flow



	Nitrate (mg/l)
Before	9.29
After	3.36
Reduction	63.8%

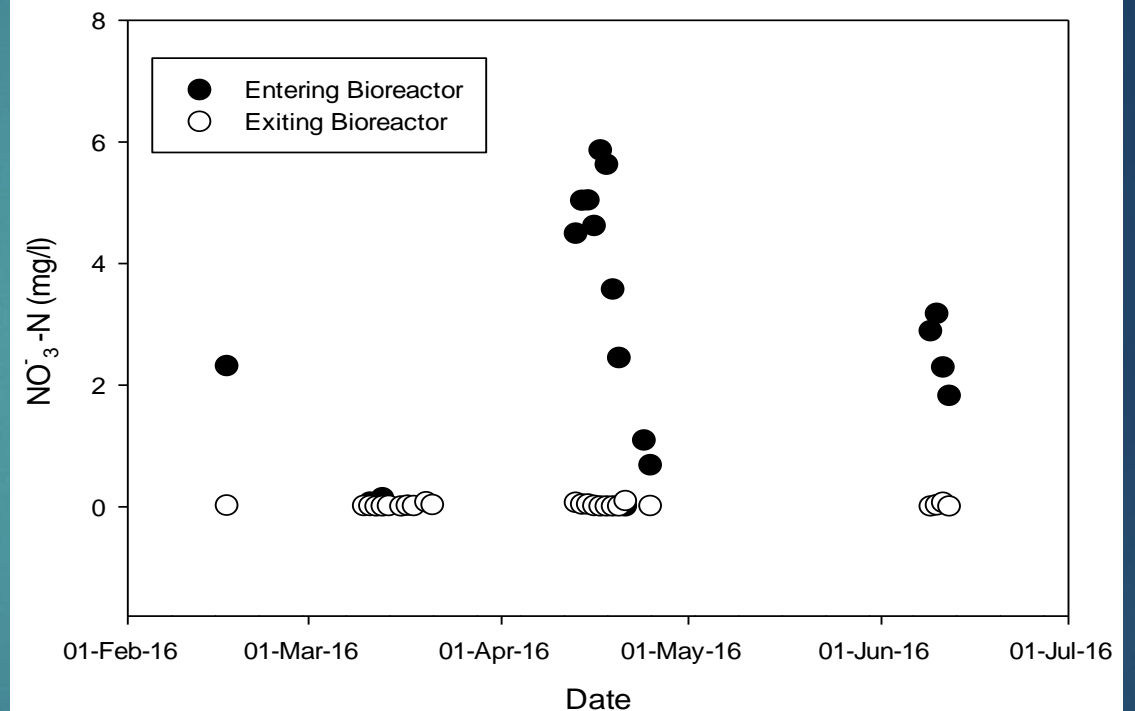
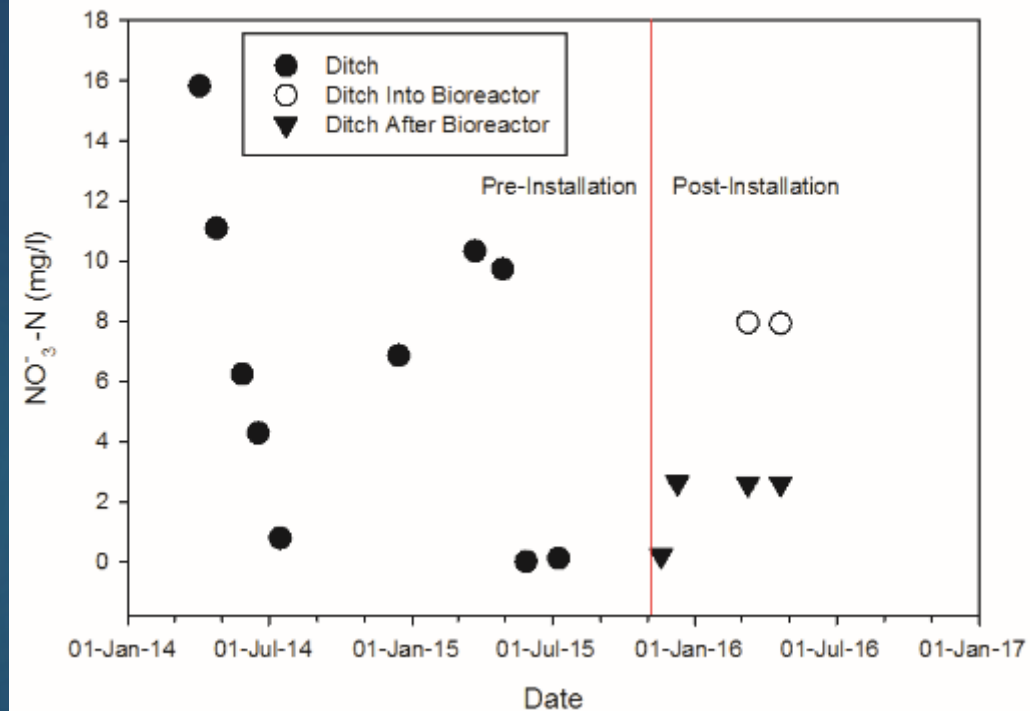


	Nitrate (mg/l)
Before	6.40
After	3.68
Reduction	42.6%

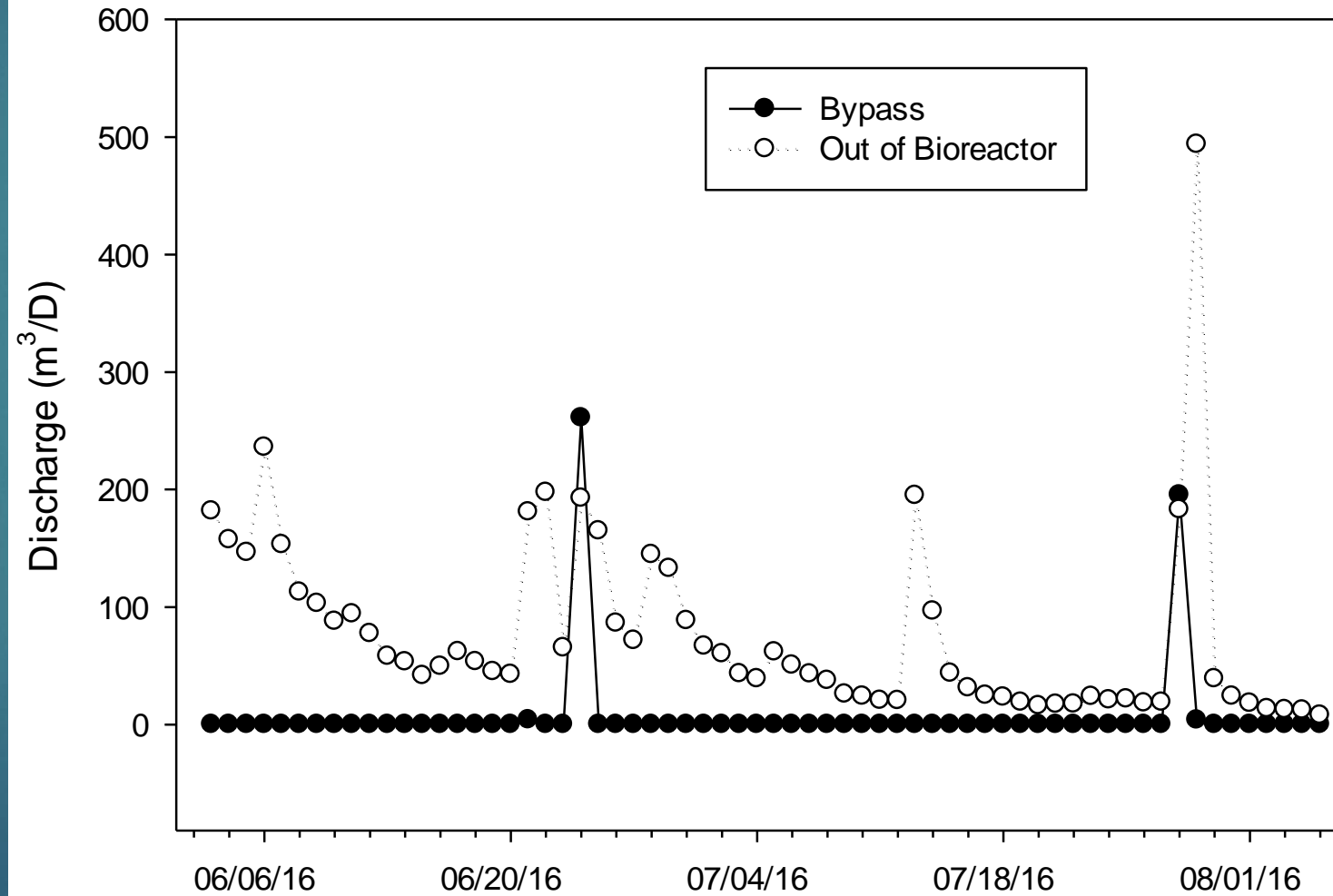




# Second Generation



# Second Generation





# Questions?

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